Attrition Dry Milling In Continuous And Batch Modes

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ABSTRACT:
This paper will try to answer the WHY, WHAT, and HOW of attrition fine dry milling using Attritors in continuous or batch type modes. The principle of Attritor dry grind processing is achieved by an expanded moving bed of media. This condition is described as kinematic porosity. The dry particles are subjected to various forces such as impact, rotational, tumbling, and shear. Therefore, micron range fine powders can be easily achieved. Additionally, combinations of these forces create a more spherical particle than other impact-type milling equipment.

The Attritor’s versatility is gained by the ability to operate under a broad range of conditions. For example, grinding media type, size, and amount; different machine speeds; variable loading or feed rate of raw material. In addition to reducing particle size, Attritors also can create the highest intensity intimate blending of dissimilar materials. Specific chemicals or additives can also be introduced to the mill during the grinding process and achieve the ultimate dispersing or coating on the dry solid particles.

WHY ATTRITOR DRY MILLING?
Process Economics: Attritors are an energy efficient, compact, easy to operate, and require low maintenance.
Versatility: Attritor design allows modification of numerous variables to adjust changing specifications and meet final product requirements.

Reduced Transportation Costs: In many wet slurry processes, 50% of the gross weight is liquid.

Energy Savings: Removal of the liquid from a wet grinding process involves not only another process step, but also requires large amounts of energy.

Eliminate Waste Liquid Disposal: Following stricter environmental regulations, the disposal of any waste liquid (water or solvent) is very costly.

WHAT ARE SOME COMMON APPLICATIONS FOR DRY GRIND ATTRITORS?
- Ceramic Powders
- Ferrite
- Glass Frits
- Pigments
- Metal Powders
- Minerals
- Mechanical Alloying
- Coal & Coke
- Metal Oxides
- Graphite
- Fibers & Cellulose
- Plastics & Rubber
- Food Products
- Chemicals

HOW DOES ATTRITOR DRY MILLING WORK?
The Attritor dry grind process is achieved in a stationary tank by means of a rotating shaft and arms that agitate the media into a random state of motion of internal porosity called “kinematic porosity”. (Fig. 1) In this expanded condition, the media and particles are free to move, collide, and impinge upon each other, thus generating high shear and powerful impact for efficient grinding. (Fig. 2)

Figure 1: Kinematic Porosity

Figure 2: Action Of Media

Dry Grind Attritor Types:
1. SDG Series
The SDG Series (“Regular” Speed Dry Grind Attritors) can be operated in continuous or batch grinding processes. In the continuous operation, the material is...
fed into the grinding chamber at the top, then falls through the agitated media bed where it is ground to desired particle size and discharged through a metering type valve assembly at the bottom of the tank. (Fig. 3)

In the batch mode, material is charged into the mill at the top, ground to the required size, then discharged through grids at the tank bottom. The SDG Attritors can easily be sealed for grinding under inert gases such as nitrogen or argon. The system can also be constructed with ceramic materials for metal-free grinding processes.

The SDG Attritors use grinding balls from 5mm to 13mm. The shaft RPM generally runs from 75 to 500. This series of Attritors are suitable for hard-to-grind materials such as metal powders, metal carbides, and glass chunks. The feed material size for these machines can be quite coarse, but smaller than the grinding media chosen.

The SDG Attritor is also used to make dispersion strengthened metal (DSM). In this process (known as mechanical alloying or cold welding), the kinematic porosity results in grinding media breaking the metals and additives into small particles first, then beating them together to form agglomerates. By repeating the process, the various metals are evenly mixed and dispersed to form a new composition of alloy (DSM).

II. HSA Series

HSA (High Speed Attritors) was newly developed in the past few years. These machines feature a unique patented design concept that includes a new grinding tank internal configuration and side discharge screen which allows mills to run at higher speed, using smaller media, and continuously discharges product out of the mill by centrifugal force. (Fig. 4)

HSA Attritors generally operate from 400-1800 RPM using grinding beads from 1-3mm. This combination of high velocity and increased grinding media surface area insure much finer grind of the processed material.

The HSA Attritor is generally used in a continuous mode. The material is charged into the mill at the top by a pre-set rate feeder, and discharged out the lower side of the grinding tank. HSA Series Attritors are generally used for finer feed material (-40 mesh), and produce large quantities of ultra fine powders in micron size. Applications include various minerals such as calcium carbonate, talc, barium sulfate, iron oxide, rice hull ash, and fynash. The HSA is also often used for ilmenite and polymer type of materials.

III. System Setup Options

The SDG and HSA Attritors also can be setup as two-stage process, using larger media in the SDG Attritor to pregrind coarse feed material, then continuously run through the HSA Attritor with mini media to achieve the final ultrafine products. (Fig. 5)

An air classifier or screen can be incorporated with SDG or HSA Attritors to form a closed grinding process loop. By constantly taking out the fine product and refeeding the oversized particles, very efficient, narrow distribution fine grinding is achieved. (Fig. 6)

ATTRITOR GRINDING MEDIA TYPES:

Selection of grinding media depends upon several factors, some of which are interrelated.

Specific gravity. In general, high density media give better results. The media should be more dense than the material to be ground. Also, highly viscous materials require media with higher density to prevent floating.

Initial feed size. Smaller media cannot easily break up large particles.

Final particle size. Smaller media are more efficient when ultrafine particles are desired.

Hardness. The harder the media the better the grinding efficiency and consequently, the longer the wear.

pH. Some strong acid or basic material may react with certain metallic media.

Discoloration. For instance, white material should remain white.

Contamination. The material resulting from the wear of the media does not affect the product or can be removed by a magnetic separator, chemically, or in a sintering process.

Cost. Media that may be 2-3 times more expensive may wear better, sometimes 5-6 times longer, therefore, well worth their
extra cost of the long run.

Following is a list of types of media used in Attritors:
- through-hardened carbon steel
- aluminum oxide
- chrome steel
- stainless
- 440C stainless steel
- tungsten carbide
- zirconium silicate
- silicon nitride
- cerium oxide (MgO or Y2O3 stabilized)
- silicon carbide

CONTINUOUS OR BATCH GRINDING PROCESS?
Batch dry grinding is employed when the material requires longer residence time (over 30 min. and more), and the prime consideration is the finest particle size possible, tighter distribution.

Another important reason for choosing batch grinding is ability to control the milling atmosphere. The grinding tank cover can be equipped with a mechanical shaft seal. Purging with inert gas allows material to grind under an oxygen free condition. A specially designed, sealed discharge container also can be equipped with the machine.

Continuous dry grinding is chosen for the following reasons:
1. Large production quantity is required.
2. Material is temperature sensitive. With continuous processing, all the material passes through the grinding chamber quickly without overheating inside the mill.
3. Material has a tendency to cake. Constantly moving material through the media bed prevents material buildup against the tank wall.

The continuous grinding process requires a stable condition to maintain inside the mill at all times. The objective is to precisely control the retention time in the mill long enough to reduce the particles to the size desired. Special accessories are used to control this process.

1. An accurate feeding system dispensing material into the top of the mill.
2. A special shaft and arm configuration plus diverter discs. These diverter discs prevent unground material from short-circuiting through the grinding chamber and discharging prematurely.

A specially designed metering discharge can be adjusted to dispense the exact amount of material from the mill as is being added to the top of the mill. The adjustable discharge also allows one to easily maintain or change the bed amount of material inside the mill.

A torque sensor fitted to the rotating shaft and display readout indicates torque in inch-pounds. By observing this torque readout and operating within a narrow range of variation, you can be assured that the material bed in the mill and process conditions are stable. As a result, all the material passing through the grinding chamber is being processed with similar amounts of grinding energy. (Fig. 7)

The results from this kind of process procedure show very tight quality control specifications. All the process data can be sent to a computer printout and used for ISO requirement documentation.

If the system is shut down overnight, it is generally not necessary to drain the material from the mill prior to start-up, since the bed of processed material already exists inside the mill, start-up involves only turning on the mill and the feeding equipment.

<table>
<thead>
<tr>
<th>MATERIAL</th>
<th>PARTICLE SIZE ORIGINAL</th>
<th>PARTICLE SIZE FINAL</th>
<th>PROCESS MODE</th>
</tr>
</thead>
<tbody>
<tr>
<td>Alumina</td>
<td>MV 10μ</td>
<td>MV 1.6μ</td>
<td>C</td>
</tr>
<tr>
<td>Coral Glaze (Fe₂O₃/ZrO₂)</td>
<td>FSS 9.4μ</td>
<td>FSS 1.6μ</td>
<td>C</td>
</tr>
<tr>
<td>Ferrite</td>
<td>+2 mesh</td>
<td>MV 4.6μ</td>
<td>B</td>
</tr>
<tr>
<td>Glass Felt</td>
<td>1&quot; Sq.</td>
<td>50% 3.2μ</td>
<td>B</td>
</tr>
<tr>
<td>Glass Ribbon</td>
<td>+3 mesh</td>
<td>50% 4.3μ</td>
<td>B</td>
</tr>
<tr>
<td>Iron Exchange Resin</td>
<td>-200 mesh bends</td>
<td>50% 1.15μ</td>
<td>B</td>
</tr>
<tr>
<td>Iron Mill Scale</td>
<td>2-3&quot; Chunks</td>
<td>FSS 2.4μ</td>
<td>C</td>
</tr>
<tr>
<td>Iron Oxide Beads</td>
<td>1/8&quot;-1/16&quot; Beads</td>
<td>FSS 1.4μ</td>
<td>C</td>
</tr>
<tr>
<td>Nickel Oxide</td>
<td>FSS 8.3μ</td>
<td>50% 4.7μ</td>
<td>B</td>
</tr>
<tr>
<td>Petroleum Cake</td>
<td>Up to 3/16&quot; Chunks</td>
<td>50% 4.7μ</td>
<td>B</td>
</tr>
<tr>
<td>Phosphates/Europian Blue Pigment</td>
<td>20-40μ</td>
<td>Color Development</td>
<td>B</td>
</tr>
<tr>
<td>Quinacridone Pigment</td>
<td>-325 mesh</td>
<td>Color Development</td>
<td>B</td>
</tr>
<tr>
<td>Silicon Metal</td>
<td>80 mesh</td>
<td>-325 mesh</td>
<td>B</td>
</tr>
<tr>
<td>Sodium Bicarbonate</td>
<td>50 mesh</td>
<td>90% 325 mesh</td>
<td>B</td>
</tr>
<tr>
<td>Synthetic Graphite</td>
<td>90% 70 mesh</td>
<td>Av. 5.7μ</td>
<td>B</td>
</tr>
<tr>
<td>Waste Bottle Glass</td>
<td>1/4&quot; Pieces</td>
<td>75.5% 165 mesh</td>
<td>C</td>
</tr>
<tr>
<td>Zircon Sand</td>
<td>40 mesh</td>
<td>Median 4.9μ</td>
<td>C</td>
</tr>
<tr>
<td>Zirconium Oxide</td>
<td>42-40 mesh</td>
<td>Median 3.15μ</td>
<td>B</td>
</tr>
</tbody>
</table>

In “Process Mode” column: C = “continuous” process / B = “batch” process.

PROCESS DATA EXAMPLES:
Data are collected from our pilot plant tests of ASDG and HSA-30. Instruments used to determine particle size include Tyler mesh sieve, Fisher sub-sieve: Micromer. and Sedigraph.

II. SDG SERIES ATTRITORS
2. HSA SERIES ATTRITORS

<table>
<thead>
<tr>
<th>MATERIAL</th>
<th>ORIGINAL</th>
<th>FINAL</th>
<th>PROCESS MODE</th>
</tr>
</thead>
<tbody>
<tr>
<td>Barium Sulfate</td>
<td>400 mesh</td>
<td>50%</td>
<td>2.82µ</td>
</tr>
<tr>
<td>CaCoy (Stearic Acid Addct)</td>
<td>90% 61.8µ</td>
<td>50%</td>
<td>2.68µ</td>
</tr>
<tr>
<td>Carbon Fiber</td>
<td>1/4&quot; Long</td>
<td>80-100µ</td>
<td></td>
</tr>
<tr>
<td>Cement Grouc</td>
<td>90% 40µ</td>
<td>50%</td>
<td>3.29µ</td>
</tr>
<tr>
<td>Channel carbon Black</td>
<td>60% 24µ</td>
<td>50%</td>
<td>2.4µ</td>
</tr>
<tr>
<td>Flyash</td>
<td>90% 128.7µ</td>
<td>50%</td>
<td>2.51µ</td>
</tr>
<tr>
<td>Hematite</td>
<td>-10 mesh</td>
<td>1/500</td>
<td>50% 4.15µ</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
<td>2/300 50% 2.8µ</td>
</tr>
<tr>
<td>Hydrated Lime</td>
<td>21.6% &lt;70 mesh</td>
<td>50%</td>
<td>4.8µ</td>
</tr>
<tr>
<td>Magnesite Owe</td>
<td>10% &lt;25 mesh</td>
<td>50%</td>
<td>3.7µ</td>
</tr>
<tr>
<td>Manganese Dioxide</td>
<td>60 mesh</td>
<td>50%</td>
<td>0.62µ</td>
</tr>
<tr>
<td>Oat Fiber</td>
<td>9% &lt;200 mesh</td>
<td>50%</td>
<td>0.62µ</td>
</tr>
<tr>
<td>Potato Powder</td>
<td>100 mesh</td>
<td>55%</td>
<td>&lt;200 mesh</td>
</tr>
<tr>
<td>Pumice</td>
<td>50% 22.5µ</td>
<td>50%</td>
<td>4.8µ</td>
</tr>
<tr>
<td>Rice Hull Ash</td>
<td>+50 mesh</td>
<td>50%</td>
<td>1.5µ</td>
</tr>
<tr>
<td>SBR Rubber Compound</td>
<td>1/4&quot; Chips</td>
<td>85%</td>
<td>&lt;325 mesh</td>
</tr>
<tr>
<td>Sodium Antimonate</td>
<td>99% 97.1µ</td>
<td>30%</td>
<td>2.5µ</td>
</tr>
<tr>
<td>Talc</td>
<td>200 mesh</td>
<td>45%</td>
<td>&lt;1µ / 61.4% &lt;2µ</td>
</tr>
<tr>
<td>Waste Pencil Core</td>
<td>2.5&quot; Long</td>
<td>99%</td>
<td>&lt;325 mesh</td>
</tr>
<tr>
<td>Wheat Bran</td>
<td>1/2&quot; x 1/4&quot; Flakes</td>
<td>99%</td>
<td>&lt;60 mesh</td>
</tr>
<tr>
<td>Wheat Fiber</td>
<td>&lt;1/8</td>
<td>70%</td>
<td>&lt;200 mesh</td>
</tr>
<tr>
<td>Wood Fiber</td>
<td>20% ±60 mesh</td>
<td>96%</td>
<td>325 mesh</td>
</tr>
</tbody>
</table>

In "Process Mode" column: C = "continuous" process / B = "batch" process.

SUMMARY: ADVANTAGES AND LIMITATIONS OF DRY GRIND ATTRITORS

ADVANTAGES
1. Fast, efficient and reliable fine grinding
2. Versatility of the process
3. Low power consumption
4. Machine tanks are jacketed for cooling or heating temperature control
5. Easy and safe to operate
6. Low maintenance
7. Compact design, small plant area required

LIMITATIONS
1. Feed material size are limited to less than 13µm for SDC Attritors, 40 mesh for HSA Attritors.
2. For most of the sub-micron superfine powders, wet grinding still is necessary.
3. Dry grinding process does generate more internal heat than wet grinding.
4. The availability of the appropriate type of material for the HSA machine parts and screen to obtain metal-free grinding.

A FEW DRY GRINDING TIPS:
1. Minimize moisture content in the raw material: high moisture content (over 5%) can cause material to cake inside the grinding chamber. Operating at higher temperature can drive off some moisture.
2. Maintain a proper material-to-media ratio: If the ratio of material-to-media is too high, the velocity and impact force of the media will be reduced and inefficient particle size reduction will result. On the other hand, if the ratio of material-to-media is too low, the media will impact itself causing wear of the media. Optimizing material and media ratio results in efficient particle size reduction.
3. Try to obtain uniform size feed material: Raw material with broad size range often results in wide size distribution final product. It also makes choices of process mode, machine type, media size, etc very difficult.
4. Add grind aid and additives: Chemical additives can be continuously added to the process while size reduction is taking place. These additives can be dry powders or liquids. Their function is to do one or more of the following:
   • Minimize the effects of moisture that may be inherent to the material processed
   • Change the electrical charge on the surface of the particle
   • Reduce negative effects of any static charge that may develop during the size reduction process
   • Act as partitioning agent between particles to prevent agglomeration
   • Function as lubricant between particles
   • Frequently there are some additives or ingredients added downstream which can be added during the milling stage and save one more process step

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